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(51) International Patent Classification 6: (11) International Publication Number: WO 98/50436 C08F 2/38 **A1** (43) International Publication Date: 12 November 1998 (12.11.98) PCT/AU98/00337 (81) Designated States: AL, AM, AT, AU, AZ, BA, BB, BG, BR, (21) International Application Number: BY, CA, CH, CN, CU, CZ, DE, DK, EE, ES, FI, GB, GE, (22) International Filing Date: 8 May 1998 (08.05.98) GH, GM, GW, HU, ID, IL, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, UA, UG, US, UZ, VN, YU, ZW, ARIPO (30) Priority Data: 8 May 1997 (08.05.97) patent (GH, GM, KE, LS, MW, SD, SZ, UG, ZW), Eurasian PO 6696 ΑU patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, (71) Applicant (for all designated States except US): UNISEARCH IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, LIMITED [AU/AU]; 221-227 Anzac Parade, Kensington, CG, CI, CM, GA, GN, ML, MR, NE, SN, TD, TG). NSW 2033 (AU). (72) Inventors; and **Published** (75) Inventors/Applicants (for US only): DAVIS, Thomas With international search report. [AU/AU]; 38 Earl Street, Randwick, NSW 2031 (AU). GILBERT, Robert [AU/AU]; Unit 77/19 Queen Street,

(54) Title: POLYMERISATION REACTIONS UNDER MINIEMULSION CONDITIONS

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(57) Abstract

2041 (AU).

A method of forming a polymer comprising: a) forming a miniemulsion including i) a monomer, ii) a non-aqueous solution including a cobalt-containing chain transfer agent, and iii) an aqueous solution; and b) reacting the miniemulsion in the presence of an initiator for a time sufficient to form the polymer.

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Polymerisation reactions under miniemulsion conditions Technical Field

The present invention relates to a method for the formation of polymers by emulsion polymerisation and in particular to the formation of polymers under miniemulsion conditions.

Background Art

Emulsion polymerisation is widely used as a commercial process to produce a variety of latexes for a range of industries. Emulsion polymerisation processes are typically used to produce high molecular weight polymers, however, in recent times the advantage of generating much lower molecular weights for specific product applications has become evident. Catalytic chain transfer has been shown to be a highly effective synthetic tool for reducing molecular weight in free-radical solution/bulk polymerisation and emulsion polymerisation.

Limitations to the use of catalytic chain transfer agents in emulsion polymerisation reactions have been identified in the prior art. Firstly, such polymerisation reactions result in a loss of catalytic activity with time. This has, for example, been noted where cobaloximes are used as catalytic chain transfer agents. In addition, it has been noted that initiators which form oxygen centred peroxide radicals have a detrimental effect on the reaction, causing destruction of the catalyst. Similar behaviour has also been seen for oxygen centred persulfate radicals. This latter problem is highly inconvenient for commercial application of the technology, as persulfates are often the initiator of choice.

The present inventors have surprisingly found that one way of addressing the problem in the prior art is to separate the chain transfer agent from the primary initiator radicals by operating the chain transfer polymerisation reaction under miniemulsion conditions.

In miniemulsion polymerisation, the initial monomer droplet size, of about 100 nm is much smaller than conventional emulsion polymerisation, which is about 1 μ m in size. Due to this size difference, particle nucleation occurs predominantly in the monomer droplets as opposed to creating a new particle phase.

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generating free radicals in an aqueous or organic phase may be used in the present invention. Suitable initiators include peroxides, persulfates, azo initiators and redox initiator systems. Preferable persulfate initiators include potassium persulfate (KPS), ammonium persulfate, sodium persulfate.

Preferable azo initiators include azobisisobutyronitrile (AIBN), azobiscyanovaleric acid and azobis(2-amidinopropane)dihydrochloride (Vazo V50™). Preferable redox initiators include a redox couple from which each member is selected from iron catalysts, sodium metabisulfite and sodium formaldehyde sulfonate. Particularly preferred are initiators that generate oxygen centred radicals such as, persulfates and peroxides.

The concentration of the initiator used will depend on many variables including temperature, monomer and other reaction conditions. The appropriate concentrations to be used falls within the skill of a formulator of polymers.

AIBN produces carbon-centred radicals while KPS produces oxygen centred radicals. When AIBN is used as initiator, it is preferably added to the aqueous phase, prior to the formation of the miniemulsion, while KPS is preferably predissolved in water and added in the miniemulsion at the reaction temperature.

The emulsion may be stabilised by the presence of a highly water-insoluble compound (hydrophobe). A possible role of the hydrophobe is to minimise the Ostwald ripening effect (diffusion of the oil phase from small to large droplets to reduce the interfacial free energy of the system). The hydrophobe is preferably contained in the non-aqueous solution. The hydrophobe may be selected from a variety of alkanes and fatty alcohols, however, it will be appreciated that a suitable hydrophobe can be selected from a wide variety of other species. Preferably the alkane is hexadecane and the fatty alcohol is cetyl alcohol

An advantage of miniemulsion polymerisation is that highly water insoluble ingredients are present directly in the monomer droplets which are the locus of polymerisation, whereas in conventional emulsion polymerisation, monomer and other reaction components need to diffuse from the droplets via the water phase to the locus of the reaction (the particles). This can be exploited by dissolving highly water insoluble chain transfer agents directly into the monomer droplets, the loci of the reaction.

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Figure 2 is a graph showing dependence of M_n vs conversion on the concentration of catalyst (COBF and COPhBF) for AIBN initiated runs.

Figure 3 is a graph showing dependence of conversion vs time on the concentration of catalyst (COBF and COPhBF) for AIBN initiated runs.

Figure 4 is a graph showing dependence of M_n vs conversion on the concentration of catalyst (COBF and COPhBF) for KPS initiated runs.

Figure 5 is a graph showing dependence of conversion vs time on the concentration of catalyst (COBF and COPhBF) for KPS initiated runs.

Modes for Carrying Out the Invention

The following Examples further illustrate the present invention.

Six examples of miniemulsion polymerisation of methyl methacrylate using two different initiators (AIBN and KPS) and two different cobalt-containing chain transfer agents (COBF and COPhBF) have been described. The recipes for the miniemulsion polymerisation reactions carried out according to Examples 2 to 5 and 7 to 8 are outlined in Tables 1 and 2.

Table 1: Typical recipe for miniemulsion polymerisation reactions

Component	Mass/g		
water	80		
sodium dodecylsulfate	0.80		
methyl methacrylate	20		
hexadecane	0.50		
initiator: AIBN or KPS	0.20		
Catalyst: COBF or COPhBF	see Table 2		

General procedure

Typically, the miniemulsion was formed by the following procedure. The surfactant, sodium dodecylsulfate (SDS), was dissolved in deionised water that was previously deoxygenated by purging with argon for one hour. The cobalt-containing chain transfer agent was dissolved in a non-aqueous solution comprising methyl methacrylate (MMA) and the hydrophobe (hexadecane), that were previously degassed by three freeze-pump-thaw cycles. The monomer solution was transferred via a cannula to the aqueous solution and initial emulsification was achieved using a magnetic stirrer.

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Table 2: Summary of Runs

Examples	Run	Initiator	Catalyst	Concentration ^{a)}
1	A1	AIBN	-	-
2	A2	AIBN	COBF	3.0
3	A3	AIBN	COBF	18
4	A4	AIBN	COPhBF	2.0
5	A5	AIBN	COPhBF	9.3
6	K1	KPS	-	-
7	K2	KPS	COBF	17
8	КЗ	KPS	COPhBF	2.0

^{a)} ppm mol/mol, equivalent to [S]/[M] x 10⁶, where [S] is the concentration of catalytic chain transfer agent and [M] is the monomer concentration.

Results from azobisisobutyronitrile (AIBN) Initiated Polymerisation

The influence of cobalt containing chain transfer agents on the miniemulsion polymerisation of MMA initiated by AIBN can be seen in Figures 2 and 3. The control polymerisation (run A1 with no chain transfer agent) produces a number average molecular weight, M_n , in the order of 10^6 which is typical of a miniemulsion polymerisation. Upon the addition of 3.0 and 18 ppm COBF the molecular weight of PMMA is drastically reduced to 87.0×10^3 and 4.41×10^3 respectively. A similar trend is noted for the COPhBF mediated reactions with an even greater reduction in molecular weight to 18.4×10^3 and 1.10×10^3 for a slightly lower concentrations of 2.0 and 9.3 ppm.

The first significant feature is that COPhBF appears to be a more effective catalyst than COBF under these conditions. This can easily be explained by the relative solubilities of the chain transfer agents in the two phases. It has been shown that COBF partitions approximately equally between the oil and water phase. Thus for the same overall catalyst concentration, the COBF concentration in the locus of polymerisation is less than the COPhBF concentration which resides exclusively in the oil phase.

Another important point to make is that all these reactions were performed in batch and in the case of COPhBF mediated polymerisation (run A4) the efficiency of the transfer process was maintained throughout the reaction to high conversion. This contrasts with previous emulsion studies

Table 3: Summary of final properties from each run

		Molecular weight Distribution Averages (MWD)			1	Average	Distribues (PSD) ^a m)	
Run	Conv ^b	M _n	M_w	PDi	D _n	$\mathbf{D_w}$	PDi	N_c
A1	0.94	828x10 ³	2.12×10^{6}	2.6	81	96	1.19	6.14
A2	0.65	87.0×10^3	171×10^3	20	96	135	1.41	3.69
A3	0.34	4.14×10^3	10.8×10^3	2.4	-	_	-	-
A4	0.92	18.4×10^3	116×10^3	6.3	85	125	4.47	5.23
A5	0.20	1.10×10^3	3.76×10^3	3.4	-	-	-	-
K1	0.99	900x10 ³	$2.3x10^{6}$	2.6	77	86	1.12	7.15
K2	0.96	157x10 ³	$436 \mathrm{x} 10^3$	2.8	71	76	1.07	9.12
K3	0.93	17.0x10 ³	$52.3x10^3$	3.1	77	84	1.09	7.15

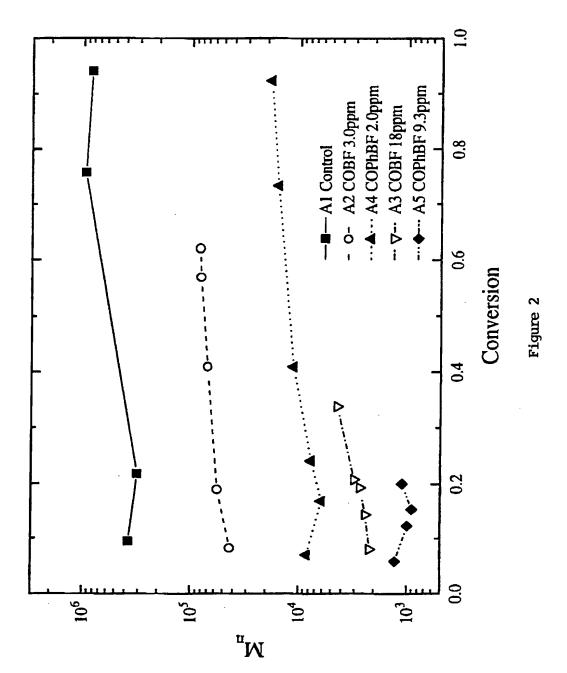
- Omitted samples did not go to high enough conversion to be measured by CHDF
- Conversion of final sample taken
- M_n Number average molecular weight
- M_w Weight average molecular weight
- PDi Polydispersity

- 10 D_n Number average diameter in nm
 - $\mathbf{D_w}$ Weight average diameter in nm
 - N_c Concentration of latex particles in L⁻¹

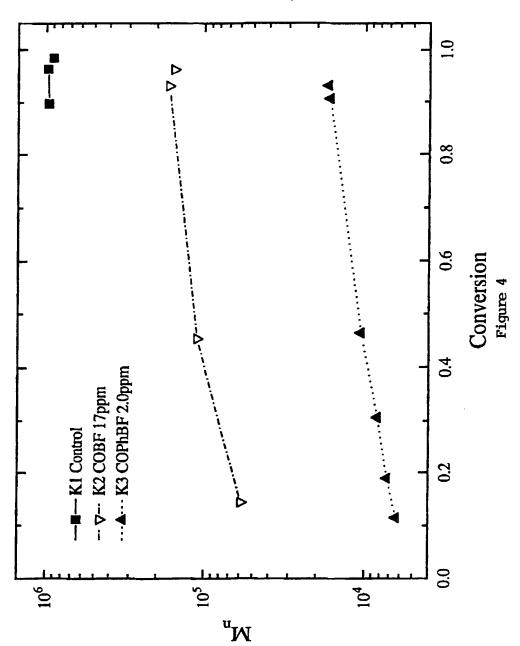
It will be appreciated by persons skilled in the art that numerous variations and/or modifications may be made to the invention as shown in the specific embodiments without departing from the spirit or scope of the invention as broadly described. The present embodiments are, therefore, to be considered in all respects as illustrative and not restrictive.

- 12. The method according to claim 11 wherein the cobalt containing chain transfer agent is tetraphenyl cobaloxime boron fluoride (COPhBF).
- 13. The method according to any one of claims 1 or 12 wherein the initiator is included prior to formation of the miniemulsion.
- 5 14. The method according to any one of claims 1 or 12 wherein the initiator is included after formation of the miniemulsion.
 - 15. The method according to any one of claims 1 or 14 wherein the initiator is selected from the group consisting of peroxides, persulfates, azo initiators, and redox initiators.
- 10 16. The method according to claims 15 wherein the persulfate initiator is selected from the group consisting of potassium persulfate (KPS), ammonium persulfate, and sodium persulfate.
 - 17. The method according to claim 15 wherein the azo initiator is selected from the group consisting of azobisisobutyronitrile (AIBN),
- azobiscyanovaleric acid, and azobis(2-amidinopropane)dihydrochloride.
 - 18. The method according to claim 15 wherein the redox initiator is selected from the group consisting of iron catalysts, sodium metabisulfate and sodium formaldehyde sulfonate.
 - 19. The method according to any one of claims 1 to 18 wherein the aqueous solution includes of one or more surfactants.
 - 20. The method according to claim 19 wherein the surfactants are selected from the group consisting of anionic, cationic and non-ionic surfactants.
 - 21. The method according to claim 20 wherein the surfactant is sodium dodecylsulfate (SDS).
- 25 22. The method according to any one of claims 1 or 21 wherein the reaction is controlled isothermally at 65°C and ambient pressure.
 - 23. A polymer prepared by the method according to any one of claims 1 to 22.

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INTERNATIONAL SEARCH REPORT

International Application No.
PCT/AU 98/00337

Α.	CLASSIFICATION OF SUBJECT MATTER					
Int Cl ⁶ :	C08F 2/38					
According to International Patent Classification (IPC) or to both national classification and IPC						
В.	FIELDS SEARCHED					
	umentation searched (classification system followed by /38, 2/40, 2/42	classification symbols)				
Documentation AU: IPC as	n searched other than minimum documentation to the e above	extent that such documents are included in	the fields searched			
	base consulted during the international search (name: EMULSION POLYMER:	of data base and, where practicable, search	ı terms used)			
C.	DOCUMENTS CONSIDERED TO BE RELEVAN	VT				
Category*	Citation of document, with indication, where ap	ppropriate, of the relevant passages	Relevant to claim No.			
A	WO 96/15158 A (E.I. DU PONT DE NEMOURS AND COMPANY et al.) 23 May 1996 A whole document					
A	EP, A, 199 436 (E.I. DU PONT DE NEMOURS AND COMPANY) 29 October 1986 Whole document					
A	1-23					
	Further documents are listed in the continuation of Box C					
* Special categories of cited documents: "A" document defining the general state of the art which is not considered to be of particular relevance "E" earlier document but published on or after the international filing date "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified) "O" document referring to an oral disclosure, use, exhibition or other means "P" document published prior to the international filing date combinated after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention document of particular relevance; the claimed invention cannot document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art document member of the same patent family						
Date of the actual completion of the international search 12 June 1998 Date of mailing of the international search report 2 2 JUN 1998						
Name and maili AUSTRALIAN PO BOX 200	Name and mailing address of the ISA/AU AUSTRALIAN PATENT OFFICE PO BOX 200 WODEN ACT 2606 AUSTRALIA HUY PHAM					



EUROPEAN SEARCH REPORT

Application Number

EP 00 00 0002

Category	Citation of document with indication of relevant passages	n, where appropriate,	Relevant to claim	CLASSIFICATION OF THE APPLICATION (int.Cl.7)
A	WO 98 50436 A (UNISEARC 12 November 1998 (1998-	H LTD) 11-12)		C08F2/22 C08F2/38
A	WO 96 15158 A (E.I.DU P CO.) 23 May 1996 (1996-	ONT DE NEMOURS AND 05-23) -		
	·			TECHNICAL FIELDS SEARCHED (Int.CI.7)
	The present search report has been d	rawn up for all claims Date of completion of the search		Examiner
	THE HAGUE	1 March 2001	Cau	wenberg, C
X : par Y : par doc A : tecl O : nor	CATEGORY OF CITED DOCUMENTS ticularly relevant if taken alone ticularly relevant if combined with another ument of the same category hnological background n-written disclosure ermediate document	T: theory or princi E: earlier patent d after the filing d D: document cited L: document cited &: member of the document	ocument, but publi ate I in the application for other reasons	ished on, or

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ANNEX TO THE EUROPEAN SEARCH REPORT ON EUROPEAN PATENT APPLICATION NO.

EP 00 00 0002

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01-03-2001

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WO 9850436	A	12-11-1998	AU CN EP ZA	7200698 A 1262692 T 0980392 A 9803881 A	27-11-1998 09-08-2000 23-02-2000 13-11-1998	
WO 9615158	A	23-05-1996	AU BR CA DE DE EP JP KR US	4147896 A 9510337 A 2205031 A 69517595 D 69517595 T 0791017 A 10508886 T 250892 B 5756605 A	06-06-1996 02-06-1998 23-05-1996 27-07-2000 15-02-2001 27-08-1997 02-09-1998 01-04-2000 26-05-1998	

For more details about this annex : see Official Journal of the European Patent Office, No. 12/82

